



A PROTOCOL FOR MODEL IDENTIFICATION IN FOOD THERMAL PROCESSING

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Computer-aided simulation offers a powerful, rational and systematic way to explain complex phenomena, evaluate hypotheses and guide new operation conditions.

AEs, ODEs, PDEs.

$$\Psi(\underbrace{\mathbf{x}}_{\text{Distributed State}}, \underbrace{\mathbf{x}_\xi, \mathbf{x}_{\xi\xi}}_{\text{Lumped State}}, \underbrace{\mathbf{v}_t, \mathbf{v}}_{\text{Controls}}, \underbrace{\mathbf{u}}_{\text{Controls}}, \underbrace{\boldsymbol{\theta}}_{\text{Parameters}}, \underbrace{\boldsymbol{\xi}, t}_{\text{Space Time}}) = 0$$

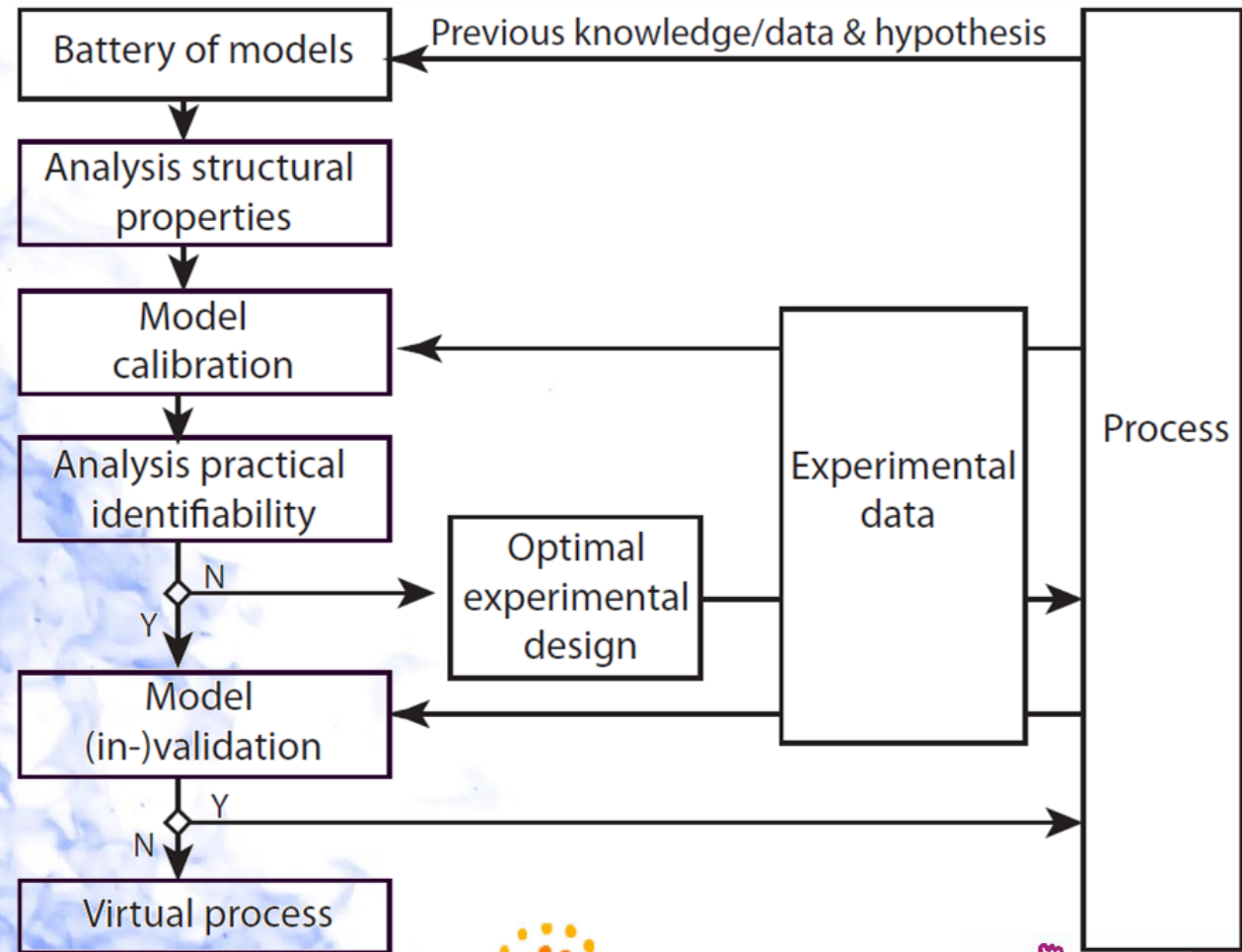
Initial conditions + Boundary conditions

How do we reconcile models with experimental data?
How can we improve model predictive capabilities?

Model identification protocol



Proposed protocol for model identification



Challenges

- Structural properties: indistinguishability, lack of identifiability

Re- formulation
Re-parameterisation
Iterative procedure

- Nonlinear models
- Large scale dynamics – Computational cost
- Medium - Large number of parameters
- The order of magnitude may be unknown
- Multimodal character of the NLP

Use of efficient and
robust simulation
and global
optimisation

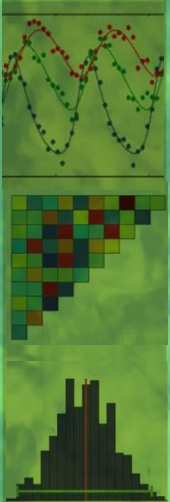
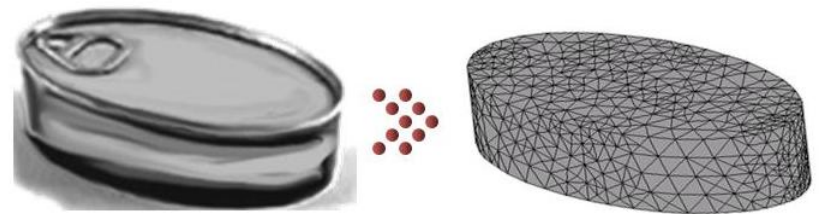
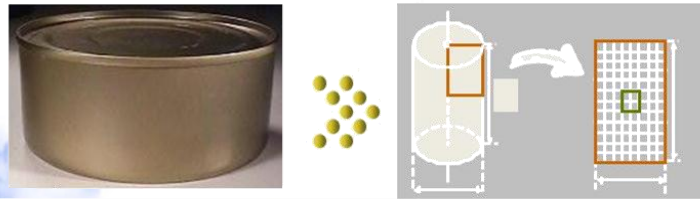
- Quantity, Quality and Variety of data
- Practical identifiability problems

Optimal experimental
design



Simulation

- Typically: spatial discretisation techniques.
- Finite elements or finite differences.
- **Reduced order modelling** offers a way to capture the essential features of the systems dynamics, with a reduced computational effort.



Model calibration

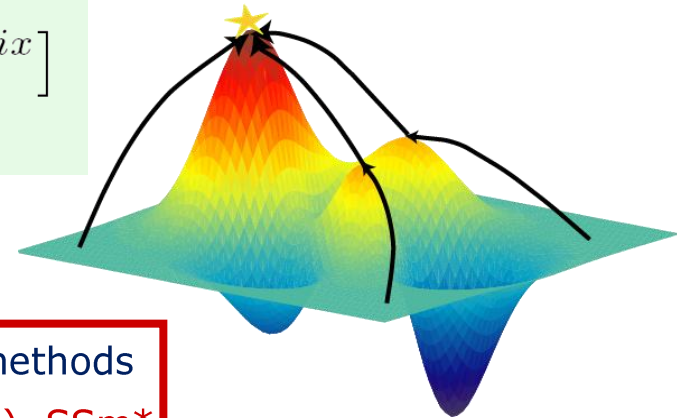
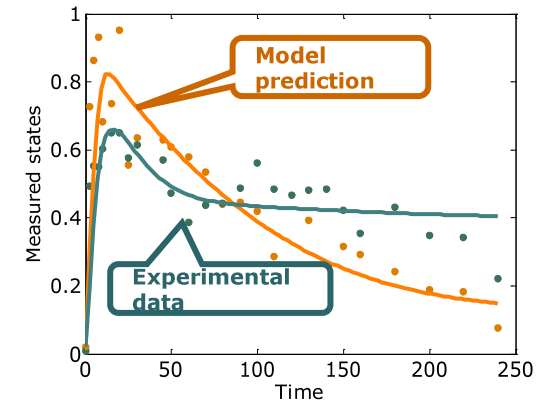
System dynamics:

$$\frac{dx}{dt} = f(x, u, v, \theta, t)$$

$$y(t_s^k, u, v, \theta) = g(x(u, v, \theta, t_s^k), \theta, t_s^k)$$

Find θ and x_0 to minimise:

$$J(\theta) = \sum_{ix=1}^{n_{exp}} \sum_{i=1}^{n_{obs}} [\Delta Y_i^{ix}]^T Q_i^{ix} [\Delta Y_i^{ix}]$$



- Local direct search and gradient based methods
- Global methods: Evolutionary (DE, SRES), SSm*

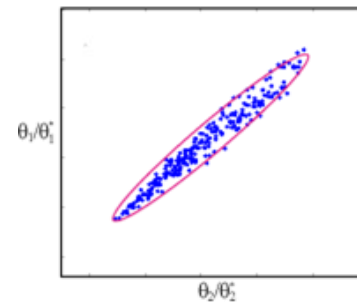
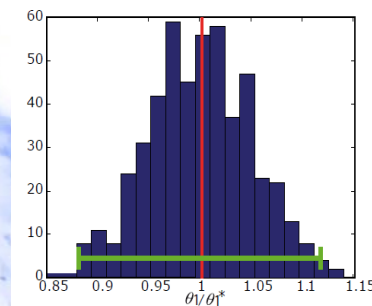
*Egea, J.A., et al (2007). J. Global Optimization 37(3):481-503.

Practical identifiability

To assess the uncertainty of the parameter estimates

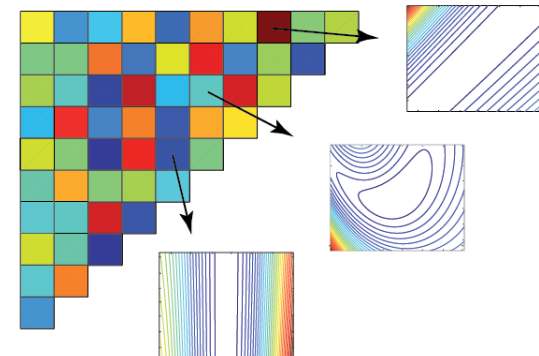
Confidence regions

Monte-Carlo based approaches



Fisher Information Matrix

$$\mathcal{F} = E_{y_m, \theta^*} \left\{ \left[\frac{\partial \mathcal{J}_{PE}(\theta)}{\partial \theta} \right] \left[\frac{\partial \mathcal{J}_{PE}(\theta)}{\partial \theta} \right]^T \right\}$$



Optimal experimental design

Calculate the dynamic scheme of measurements so as to generate the maximum amount and quality of information for model calibration purposes.

$$J_{OED} = \phi(\mathcal{F})$$

Subject to the system dynamics:

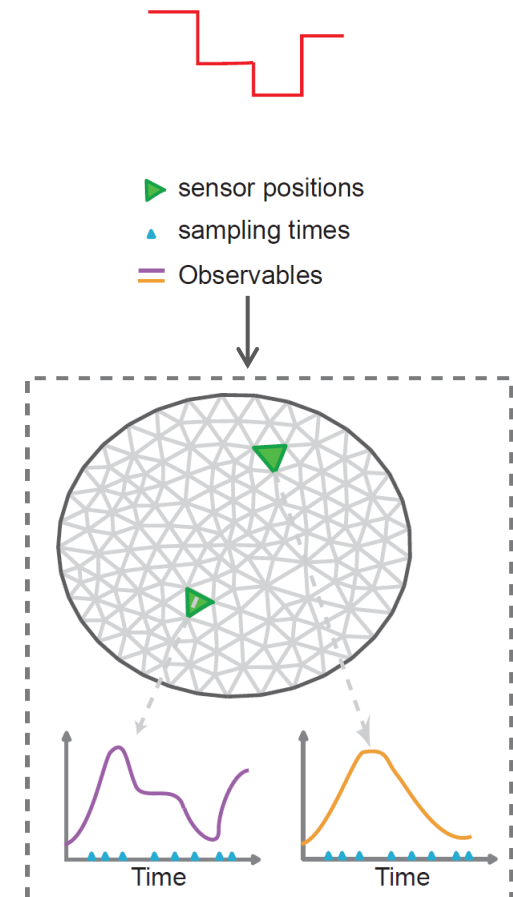
$$\frac{d\mathbf{x}}{dt} = \mathbf{f}(\mathbf{x}, \mathbf{u}, \mathbf{v}, \boldsymbol{\theta}, t)$$

$$\mathbf{y}(t_k, \mathbf{u}, \mathbf{v}, \boldsymbol{\theta}) = \mathbf{g}(\mathbf{x}(\mathbf{u}, \mathbf{v}, \boldsymbol{\theta}, t), \boldsymbol{\theta}, t)$$

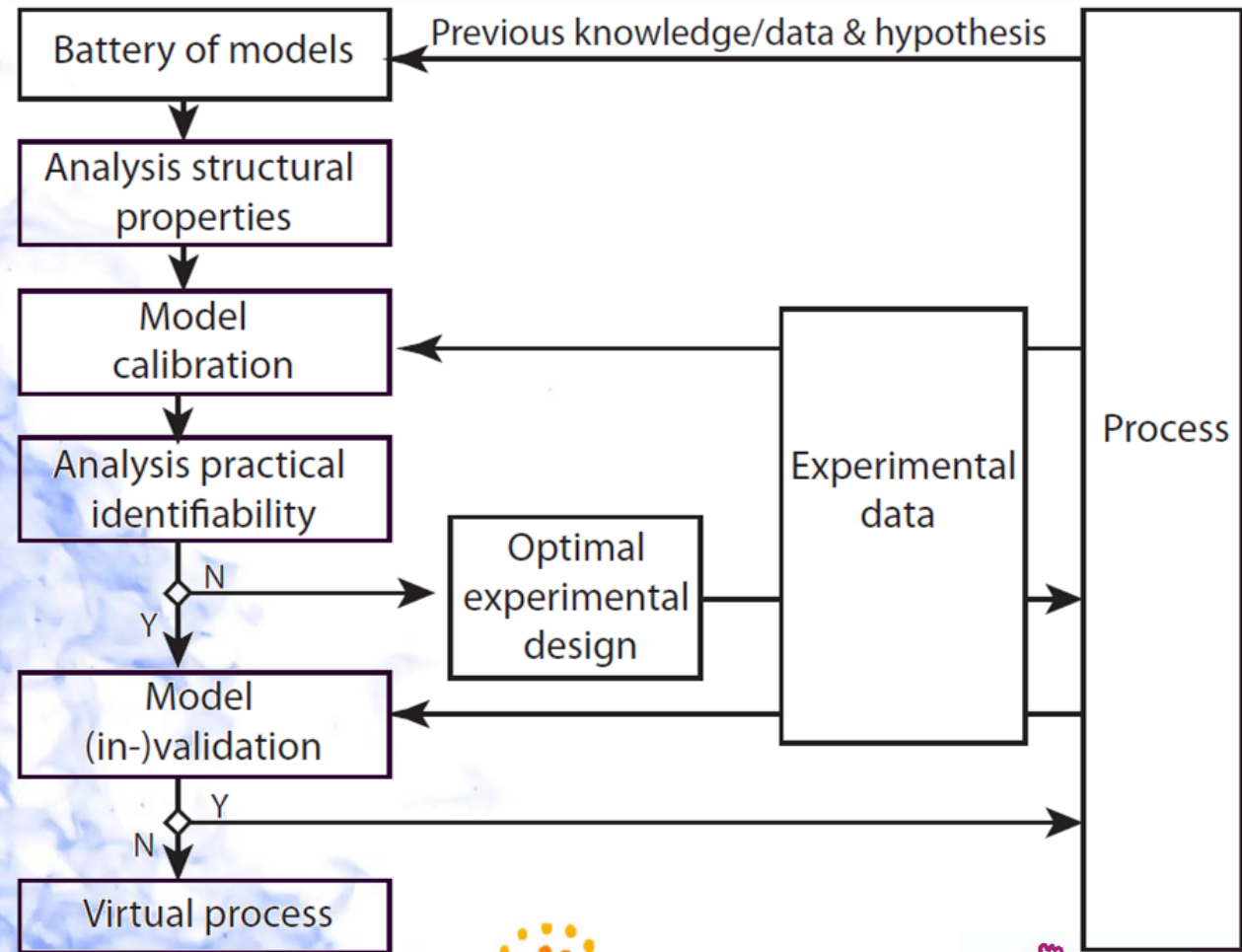
And experimental constraints:

$$\mathbf{u}^L(t) \leq \mathbf{u}(t) \leq \mathbf{u}^U(t)$$

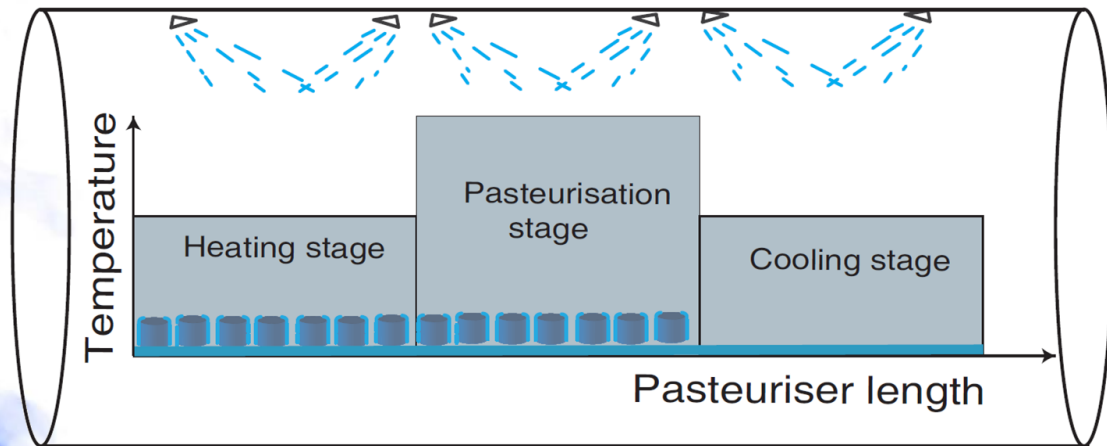
$$\mathbf{v}^L \leq \mathbf{v} \leq \mathbf{v}^U$$



Proposed protocol for model identification



Example I: Tunnel pasteurisation



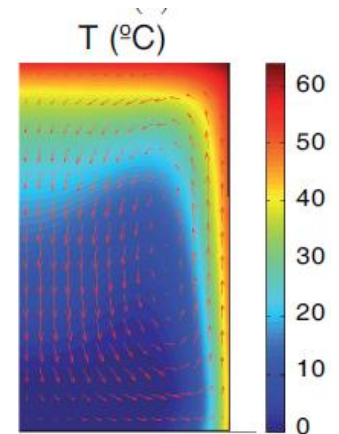
$$\nabla \vec{u} = 0.$$

$$\frac{\partial T}{\partial t} = \alpha \Delta T - \vec{u} \nabla T,$$

$$\rho \frac{\partial u}{\partial t} = \mu \Delta u - \rho \vec{u} \nabla u - \nabla P,$$

$$\rho \frac{\partial v}{\partial t} = \mu \Delta v - \rho \vec{u} \nabla v - \nabla P + \rho g \beta (T - T_0),$$

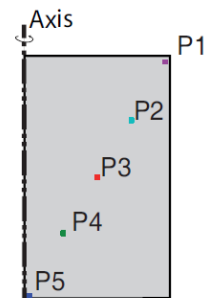
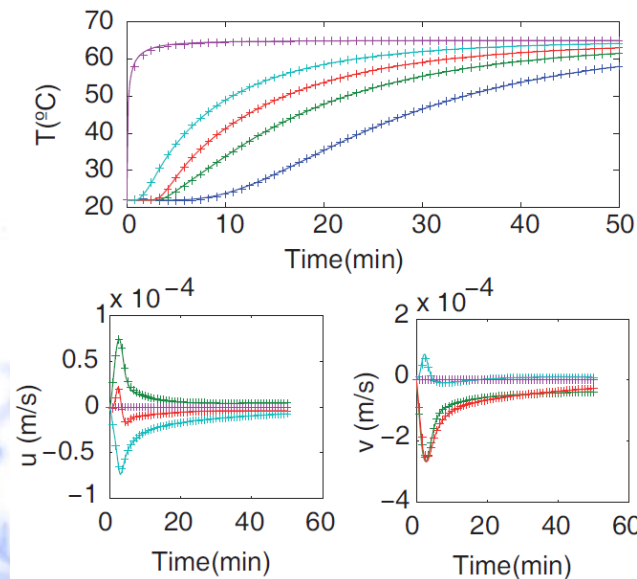
$$\frac{dP^m}{dt} = 10^{\frac{\bar{T}(t) - T_{ref}}{Z_{ref}}}$$



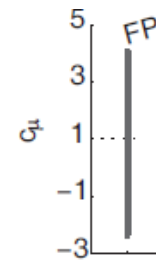
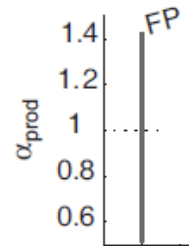
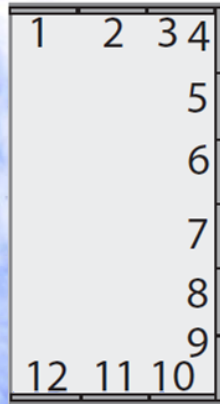
Problem I: Model simulation

PE and OED with AMIGO linked to ROM obtained by POD

Simulation method	Number of ODEs	Mean error T [%]		Mean error $\ \vec{u}\ $ [%]		Simulation time [s]
		Exp 1	Exp 2	Exp 1	Exp 2	
FEM	2900	-	-	-	-	25
ROM	10	1.08	0.75	4.3	2.61	3.1
	20	0.7	0.46	2.7	1.9	3.5
	40	0.47	0.12	1.82	0.65	4.2
	100	0.47	0.08	1.58	0.53	6.5

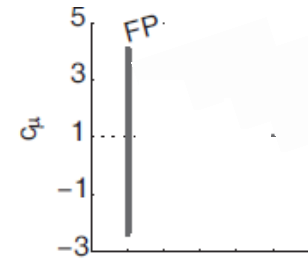
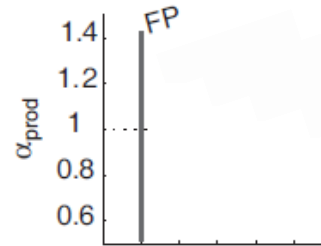
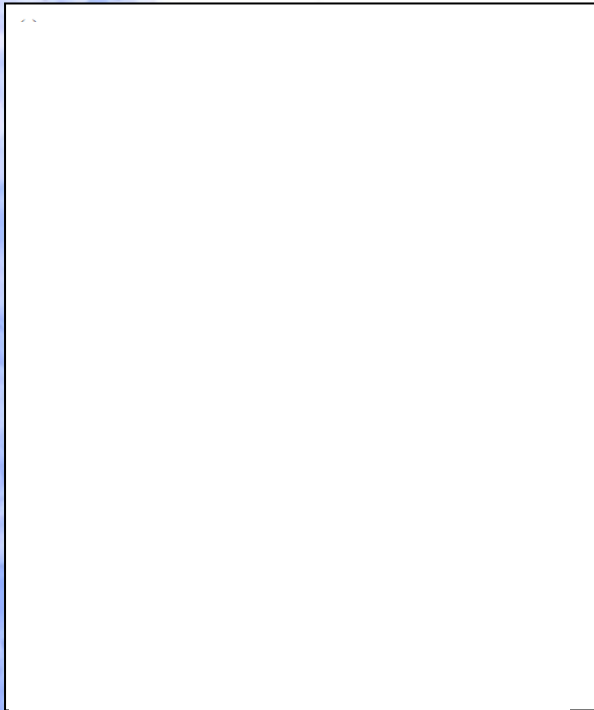


Problem I: Sensor calibration



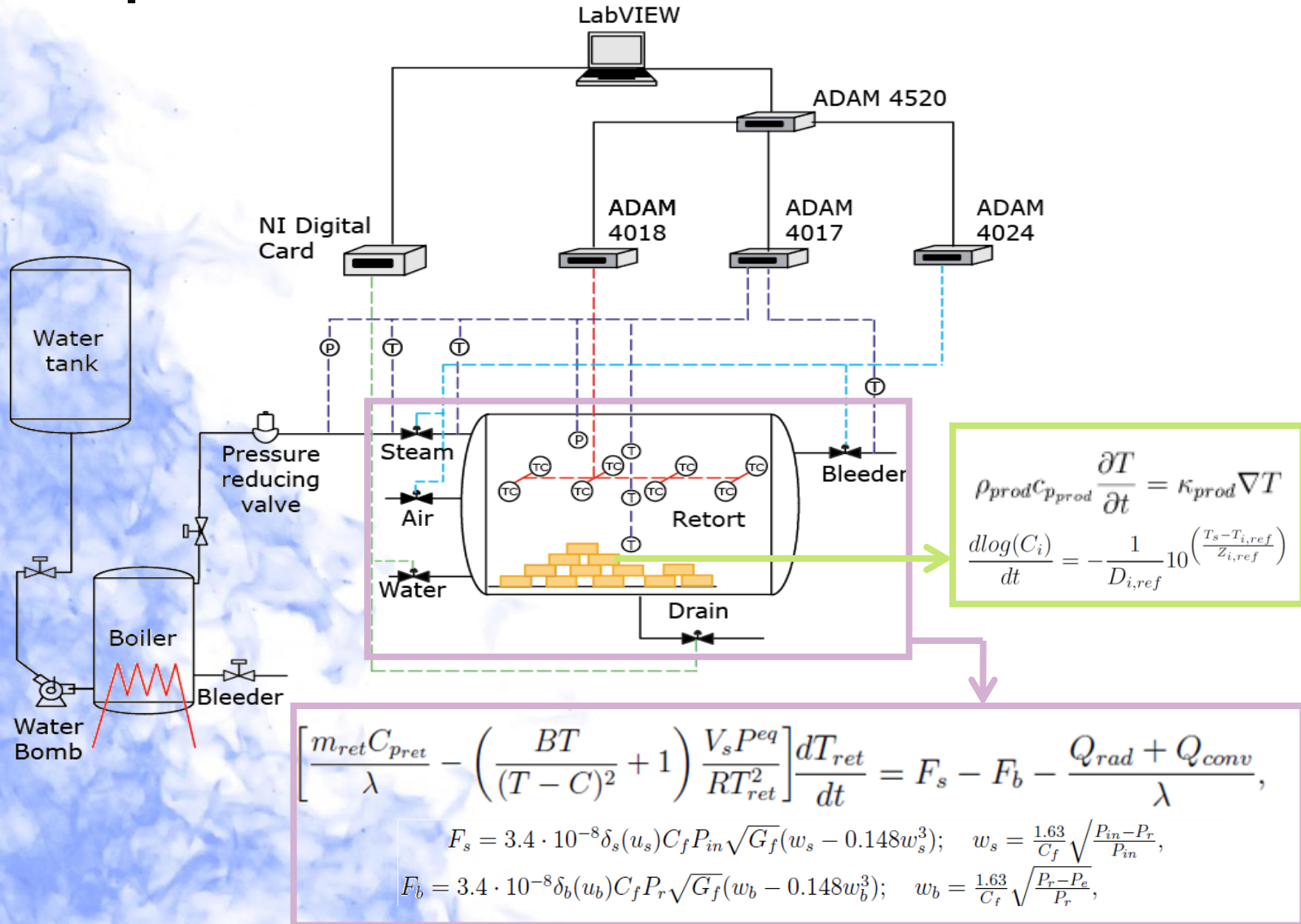
	h_{jar} [$\frac{W}{m^2K}$]	α_{prod} [m^2/s]	β []	a_μ []	b_μ []	c_μ []	mean CI	max CI
FP	0.92	0.97	1.33	0.84	0.94	0.87	251%	545%

Problem I: Sensor calibration



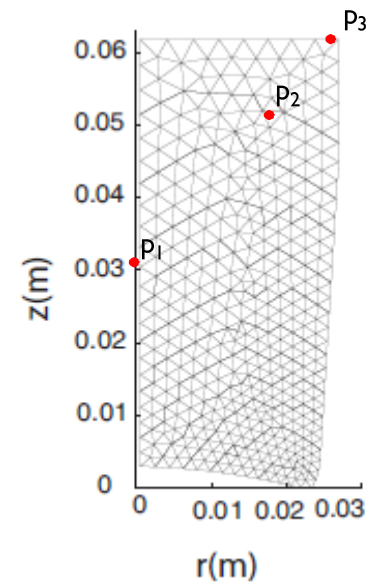
	h_{jar} [$\frac{W}{m^2K}$]	α_{prod} [m^2/s]	β []	a_μ []	b_μ []	c_μ []	mean CI	max CI
FP	0.92	0.97	1.33	0.84	0.94	0.87	251%	545%
FP+1OD	1.02	0.88	2.74	1.19	0.81	1.20	94%	210%
FP+2OD	1.01	0.97	1.55	1.17	0.81	1.03	45%	104%
FP+3OD	1.01	0.98	1.47	0.96	0.85	1.07	12%	27%
FP+4OD	1.01	0.99	1.02	1.08	1.00	1.01	1%	2.3%

Example II: Retort sterilisation



Problem II: Product model identification

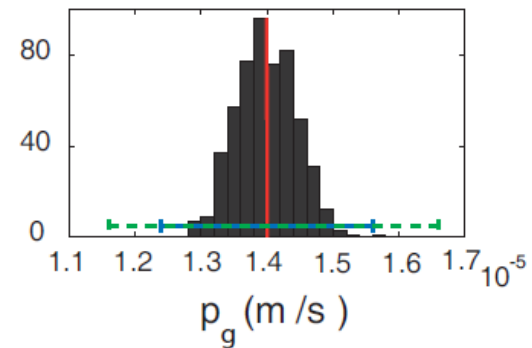
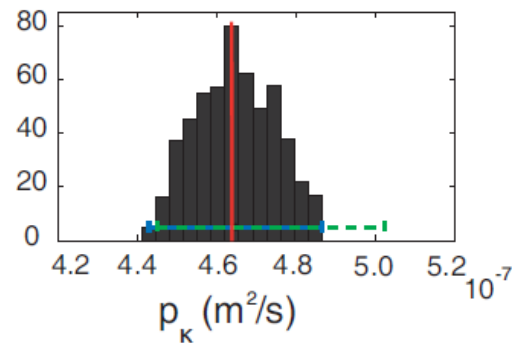
PE and OED with
AMIGO linked to ROM
obtained by POD



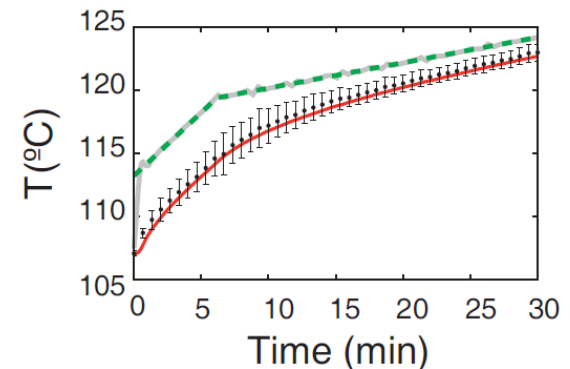
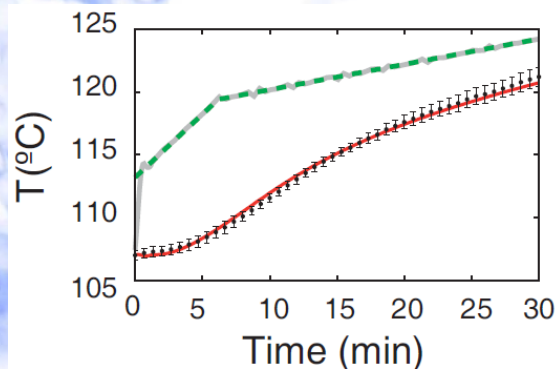
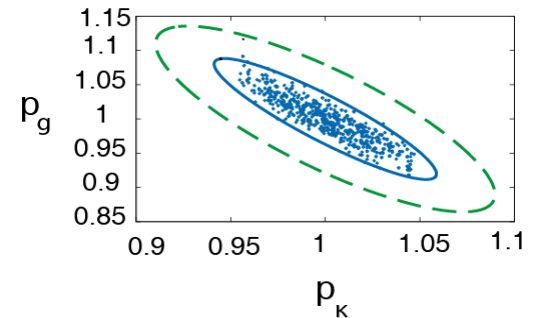
*Thermo-physical properties of food product plus
package heat transfer parameters*



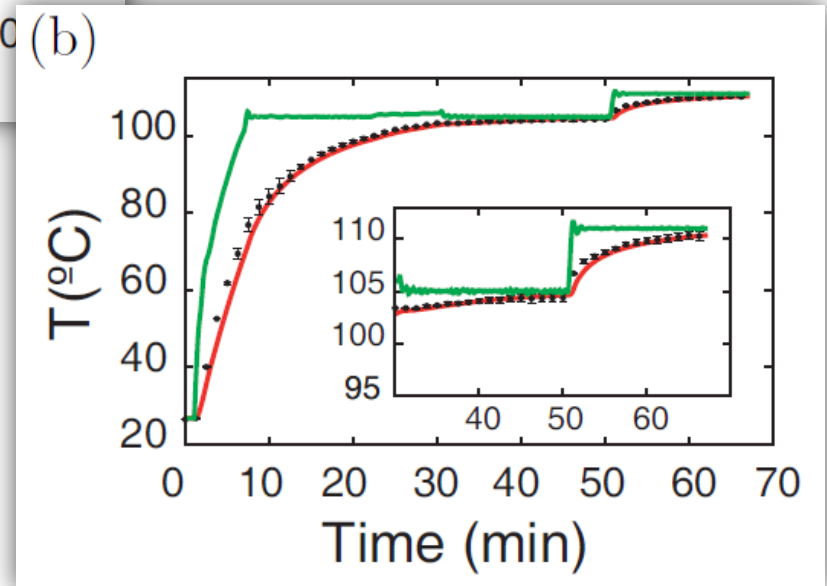
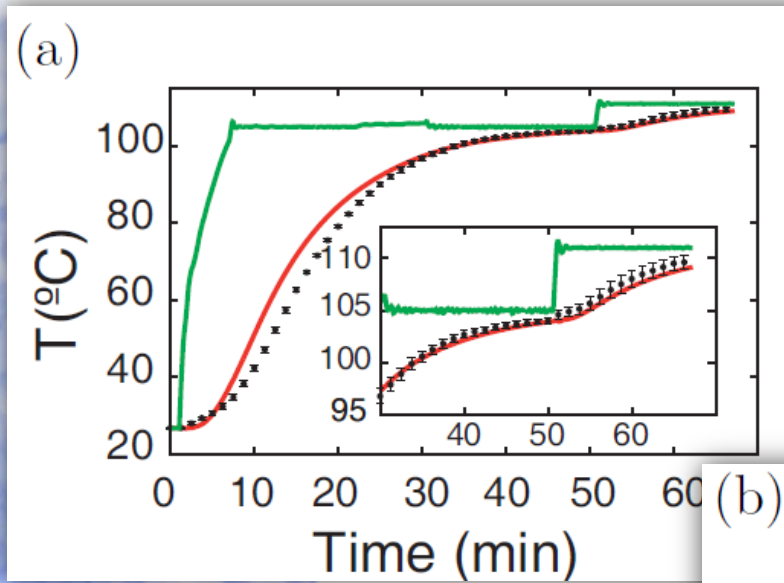
Problem II: Product model identification



*First 3 constant
temperature
Optimally
designed
experiments
were carried out.*



Problem II: Experimental validation in pilot plant



Conclusions

◈ **An iterative identification protocol for nonlinear dynamic models of food processes was presented and its performance evaluated with several examples.**

◈ **The protocol is intended to iteratively improve predictive capabilities of models.**

◈ **Key steps: Structural, practical identifiability analysis, parameter estimation and optimal experimental design.**

◈ **Key elements: Sensors + data**

Reduced order model techniques

Global optimisation methods

Software: GenSSI + AMIGO



Acknowledgments

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◊ Spectrafish.

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Thank you !